



UNIVERSITY OF  
**REGINA**

***“CO<sub>2</sub> CAPTURE AND EXACTION USING REACTIVE  
AMINES AND FORMULATED SOLVENTS”***

***INTERNATIONAL TEST CENTRE FOR CO<sub>2</sub> CAPTURE (ITC)  
University of Regina, CANADA***

***[www.co2-research.ca](http://www.co2-research.ca)***

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***[www.co2-research.ca](http://www.co2-research.ca)***

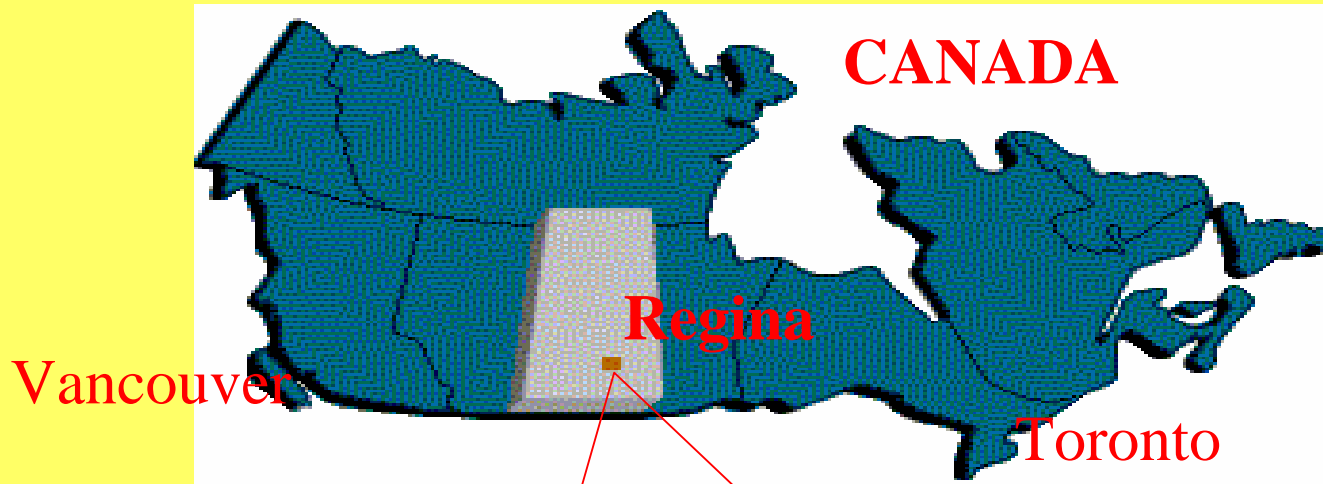
# Outlines

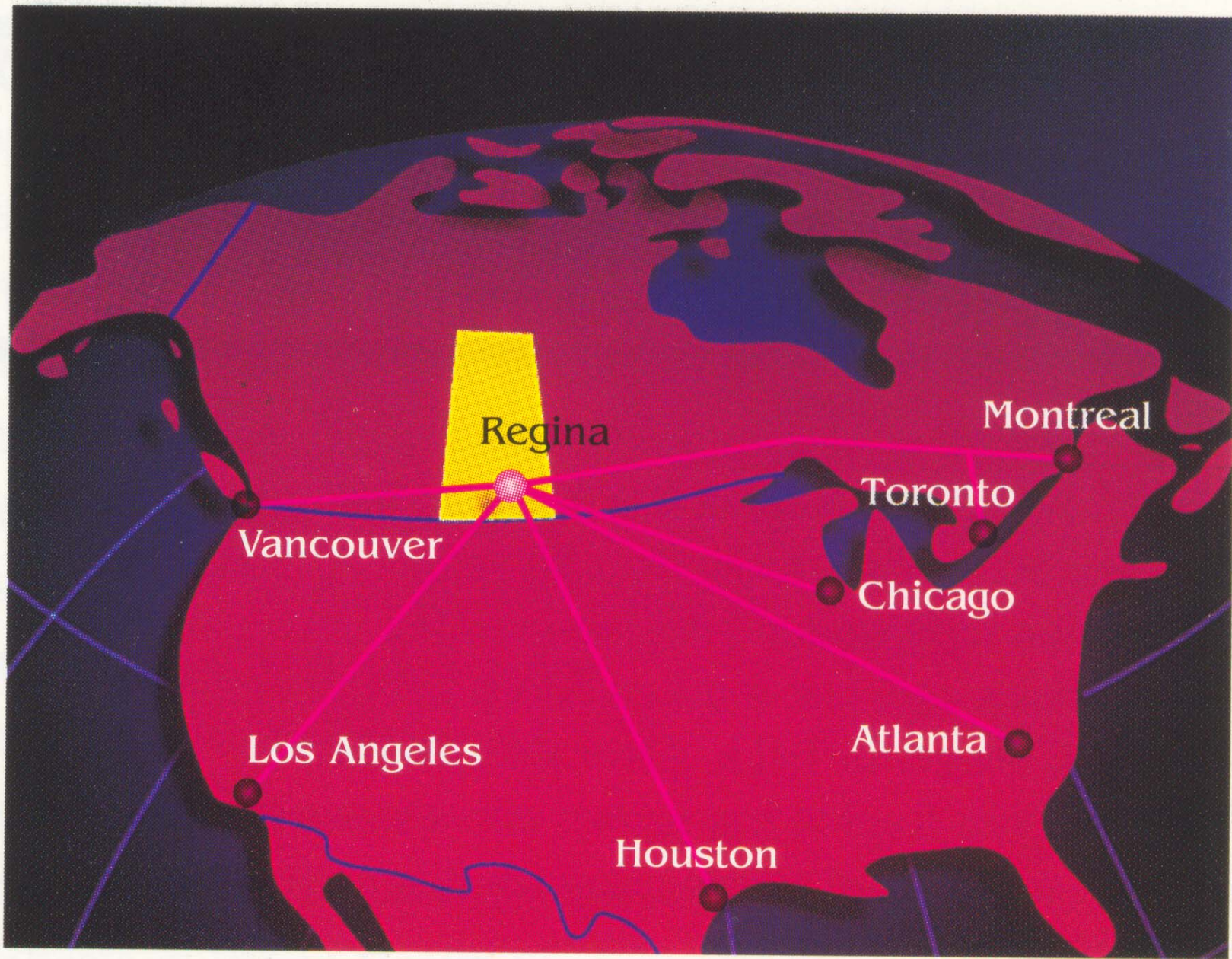
- *Background information*
- *Pilot plants and research facilities*
- *Research team*
- *Selected results (ITC Phase I)*
- *Current and future work plan (Phase II)*
- *Fundamental research at ITC*
- *Discussions*



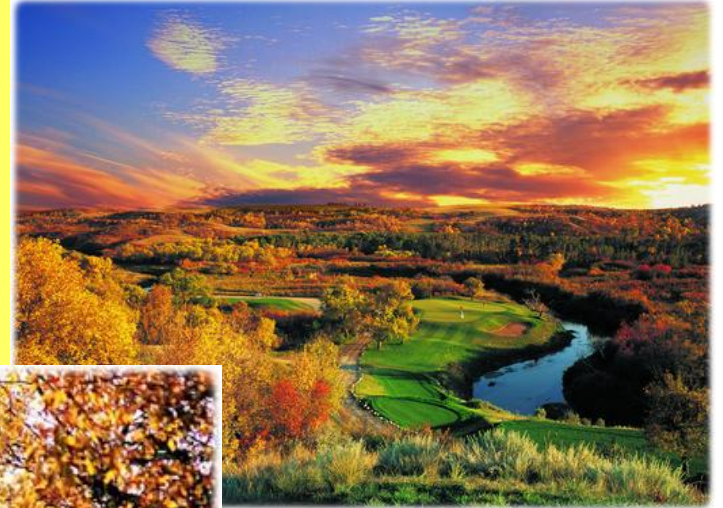
# International Test Center for CO<sub>2</sub> Capture (ITC)

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# ***REGINA, SASKATCHEWAN, CANADA***



# U of Regina's Strategic Goals

- *“Energy and Environment”* one of the key important strategic research goals
- Major strength in Climate Change Research
- Develop research excellence:
  - Prairie Adaptation Research Collaborative (PARC)
    - [www.parc.ca](http://www.parc.ca)
  - Petroleum Technology Research Centre (PTRC)
    - [www.ptrc.ca](http://www.ptrc.ca)
  - IEA Weyburn Monitoring Program for CO2 EOR & Storage
    - [www.ptrc.a](http://www.ptrc.a)
  - ITC – CO2 capture Development Program
    - [www.co2-research.ca](http://www.co2-research.ca)
  - Hydrogen & Bio-fuel Research Program ([www.htcenergy.ca](http://www.htcenergy.ca))

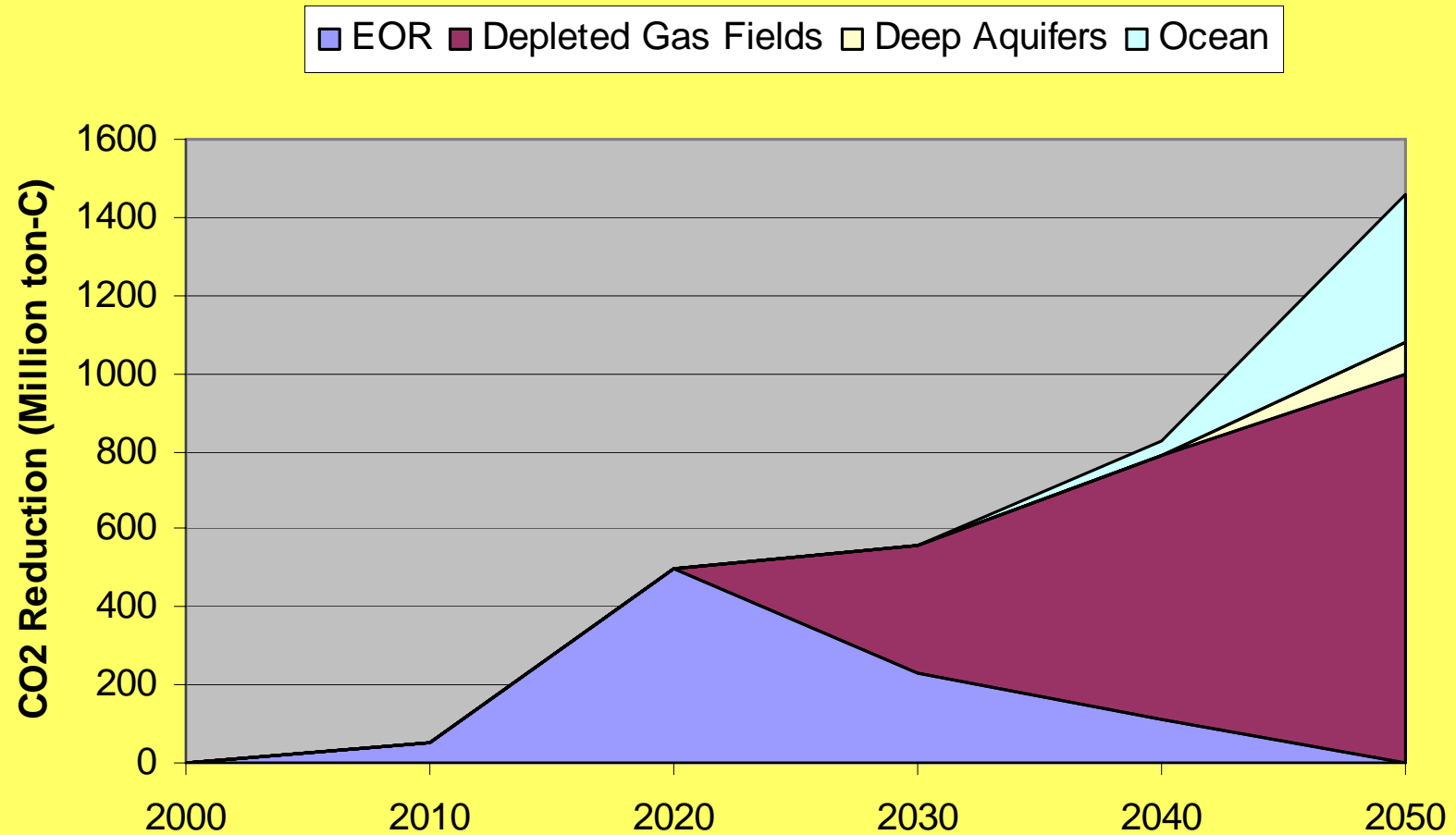
# CO<sub>2</sub> Mitigation Options

- Pre combustion
  - Energy efficient systems
  - Renewable Energy sources
  - Non-carbon fuels
  - Etc.
- Post combustion
  - **Carbon dioxide capture**
  - **Carbon dioxide Storage**
  - Carbon dioxide conversion
  - Etc.

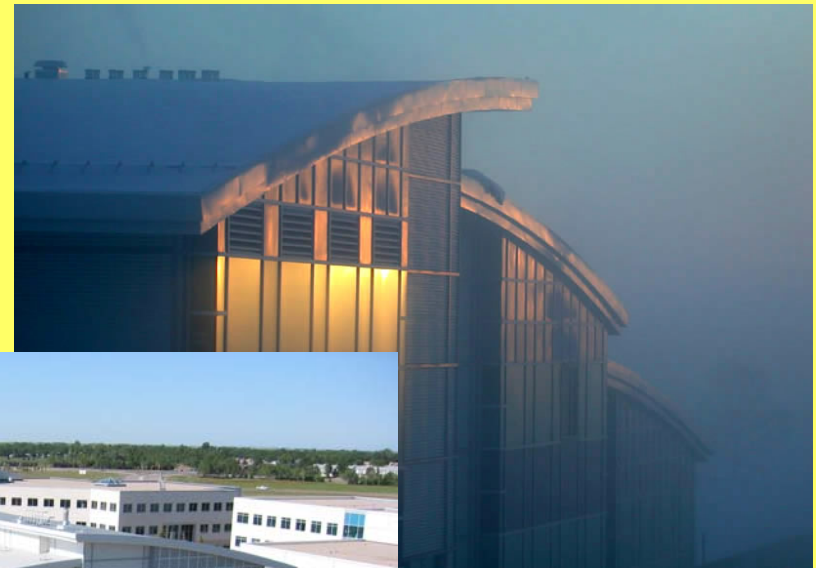


# DNE-21 Model Predictions (Kaya, 1994)

## CO2 Disposal Options



# The International Test Centre For Carbon Dioxide Capture



# GREENHOUSE GAS TECHNOLOGY CENTRE (GTC)

U of R Process Systems  
Laboratory  
(Fundamental Research)

International Test Centre  
for CO<sub>2</sub> Capture  
(ITC)

CFI

Sponsored  
Research:

*ITC –  
Industry  
Consortium*

Contract  
Research

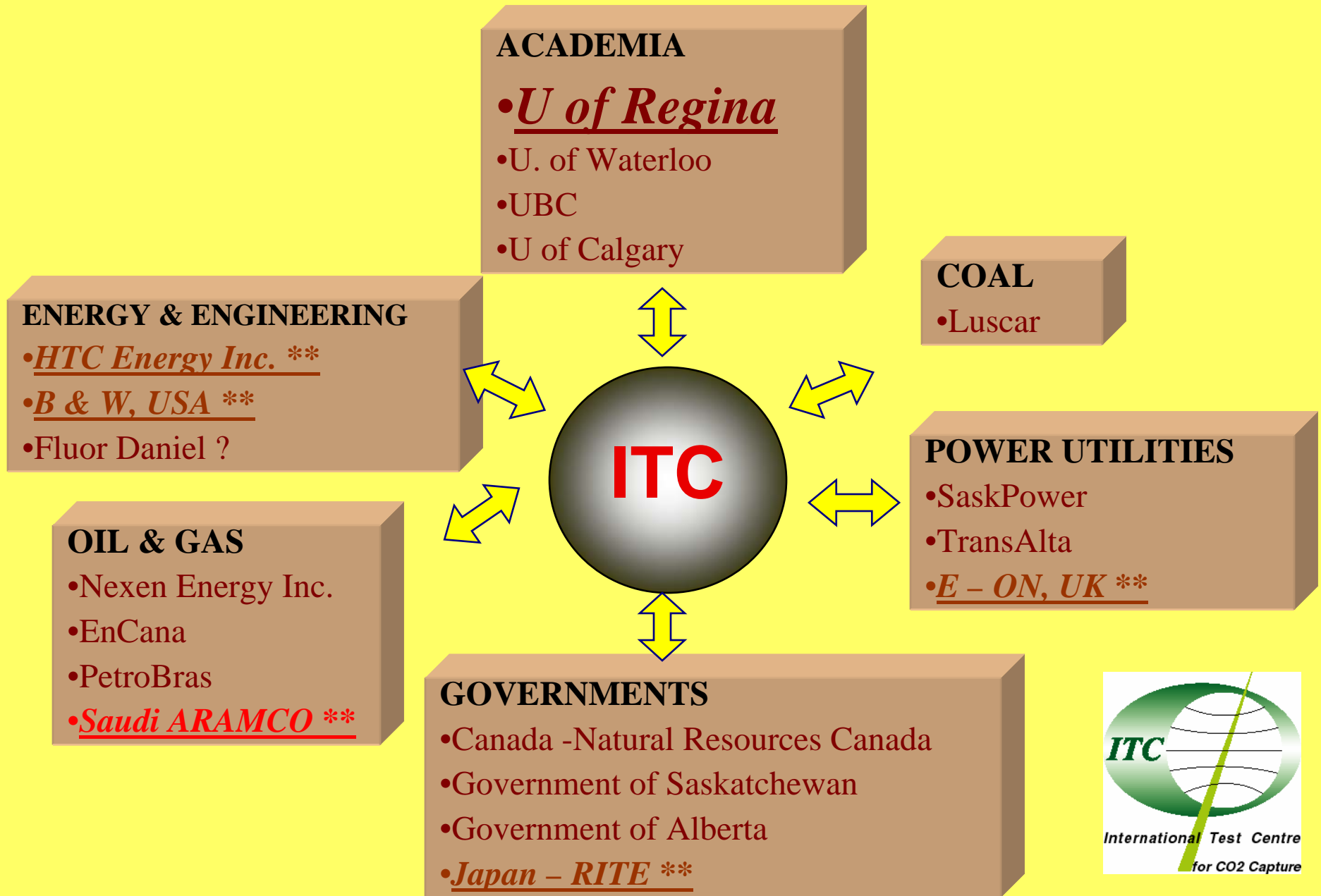
University  
Research



UNIVERSITY OF  
REGINA



# Partnerships Across Sectors



# Potential New Members

- China
- Mexico
- Korea
- SNC
- *More new members are welcome.*
- Etc.



# ITC Unique Features

## Testing Facilities

Technology Demonstration Pilot Plant:

*(CO<sub>2</sub> capture pilot unit at Boundary Dam Power Station near Estevan)*

Multi-Purpose Technology Development Pilot Plants:

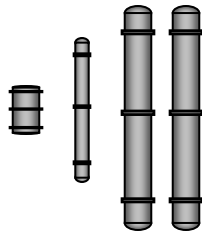
*(at University of Regina)*

Research Facilities:

*(at University of Regina)*

### U of R Research Facilities

(Absorption units / reactors)



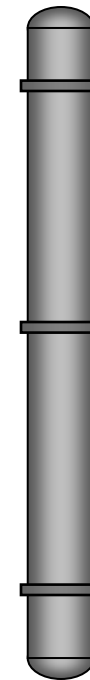
### U of R Technology development

(10-m H×12 in. ID)  
(10-m H×18 in. ID)

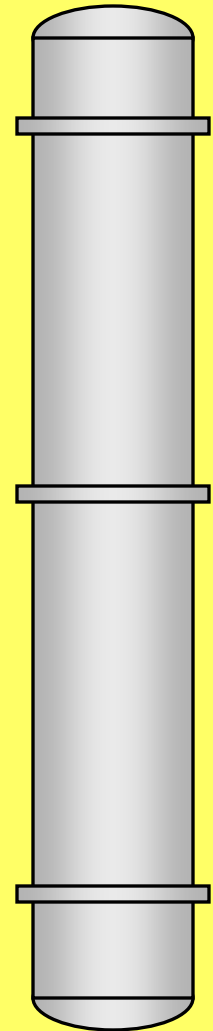


### Boundary Dam Semi-commercial testing

(20-m H×18 in. ID)



Commercial unit



# ITC Recent Investments

- ❖ Over 20 million funding has been invested in ITC's research infrastructures
  - *\$5.2 million pre-commercial scale demonstration plant at Boundary Dam*
  - *\$3.3 million Multi-purpose Technology Development Plant at the U of R*
  - *\$1.2 million bench scale facilities at the U of R*
  - *\$4.5 million analytical and computer facility from Canada Foundation for Innovations (CFI)*
  - *\$5 million from NSERC general grants over the past 10 years*

# *Technology Demonstration Plant*

## Objectives:

- To test the technical and economic feasibility of a promising process prior to commercialization.
- To evaluate the possibility for process integration with the overall system.
- To evaluate the economic feasibility of various chemicals and components proposed after laboratory and pilot-plant studies.



## BOUNDARY DAM UNIT

- Coal-fired flue gas
- Capacity - 4 - 8 ton / day of CO<sub>2</sub> (99% +)
- Flue gas flow rate - 500,000 scf / day
- ID = 18"
- Height = 20 m

*Boundary Dam Pilot Plant*



# Multipurpose Technology Development Pilot Plant



# *Key Researchers*

- *11 Key researchers + 50 Research Staff*
  - *Dr. Paitoon (PT) Tontiwachwuthikul*
  - *Dr. Amit Chakma*
  - *Dr. Malcolm Wilson*
  - *Dr. Gordon Huang*
  - *Dr. Raphael Idem*
  - *Dr. David De Montigny*
  - *Dr. Amy Veawab*
  - *Dr. Amr Henni*
  - *Dr. Andy Aroonwilas*
  - *Dr. Nader Mahinpy*
  - *Dr. Ahmed Adoudhier*
  - ❖ *Plus 50+ Researchers (Engineers, PDF's, Master & Ph.D. Students, Technical Support staff, etc.)*



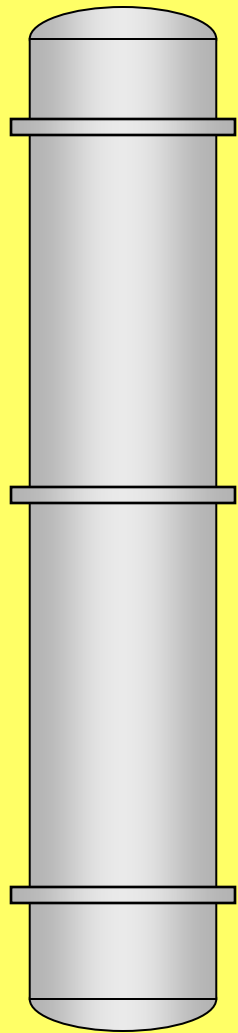
*Research  
Team*



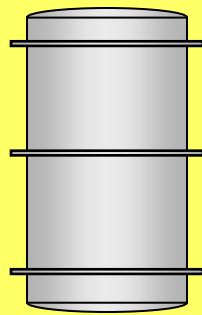
# Our Ultimate Goals



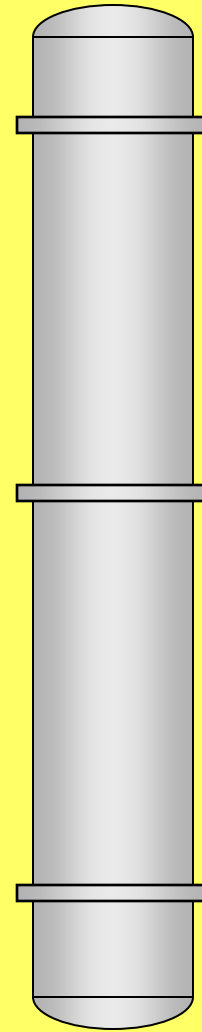
**Base Case**



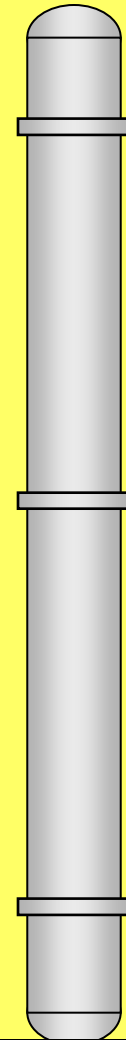
**1. Increase mass transfer of packing by 4 times**



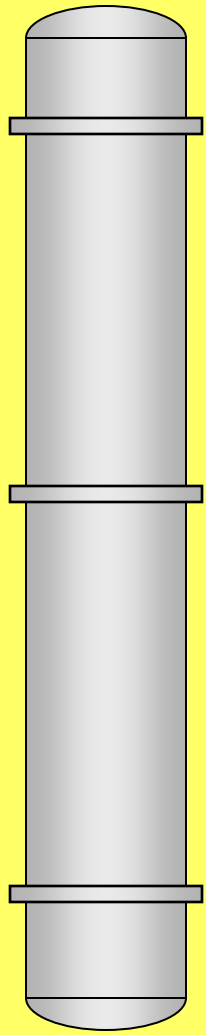
**Base Case**



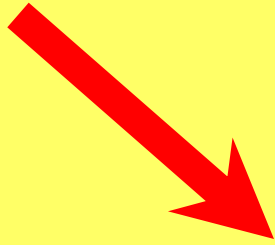
**2. Increase the solvent separation capacity by 4 times**



Base Case



R  
&  
D



*Improved  
packing  
and solvent  
- Combine  
effect ?*



???

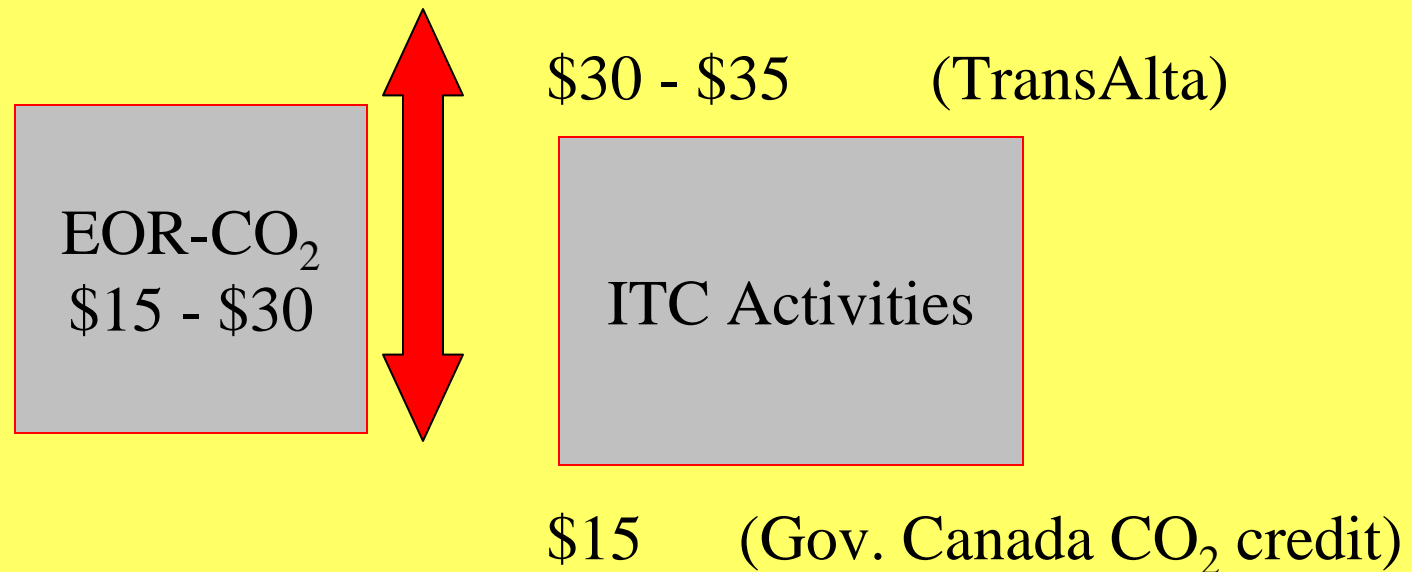


## Major Goal:

- Cost reduction for CO<sub>2</sub> capture

## Where are we?

- Capture cost: \$ 50 per ton CO<sub>2</sub> (AOSTRA Report)



# Current Status of Technology

- Reactive solvents (5 to 9 Molar)

*% Reduction*

*Energy Consumption:*



## Combined Effects

- ❑ Solvent circulation: Reduced by 50 - 60%
- ❑ Column size: Reduced by 50% (packing volume)

### Potential Cost Saving (Rough estimated)

- ❑ US\$ 30 (Based)
    - ❑ US\$15 (Capital) ..... 75% ..... US\$ 12.5
    - ❑ US\$15 (Operation) .... 50% ..... US\$ 7.5
- US\$ 20 ± \$5
-

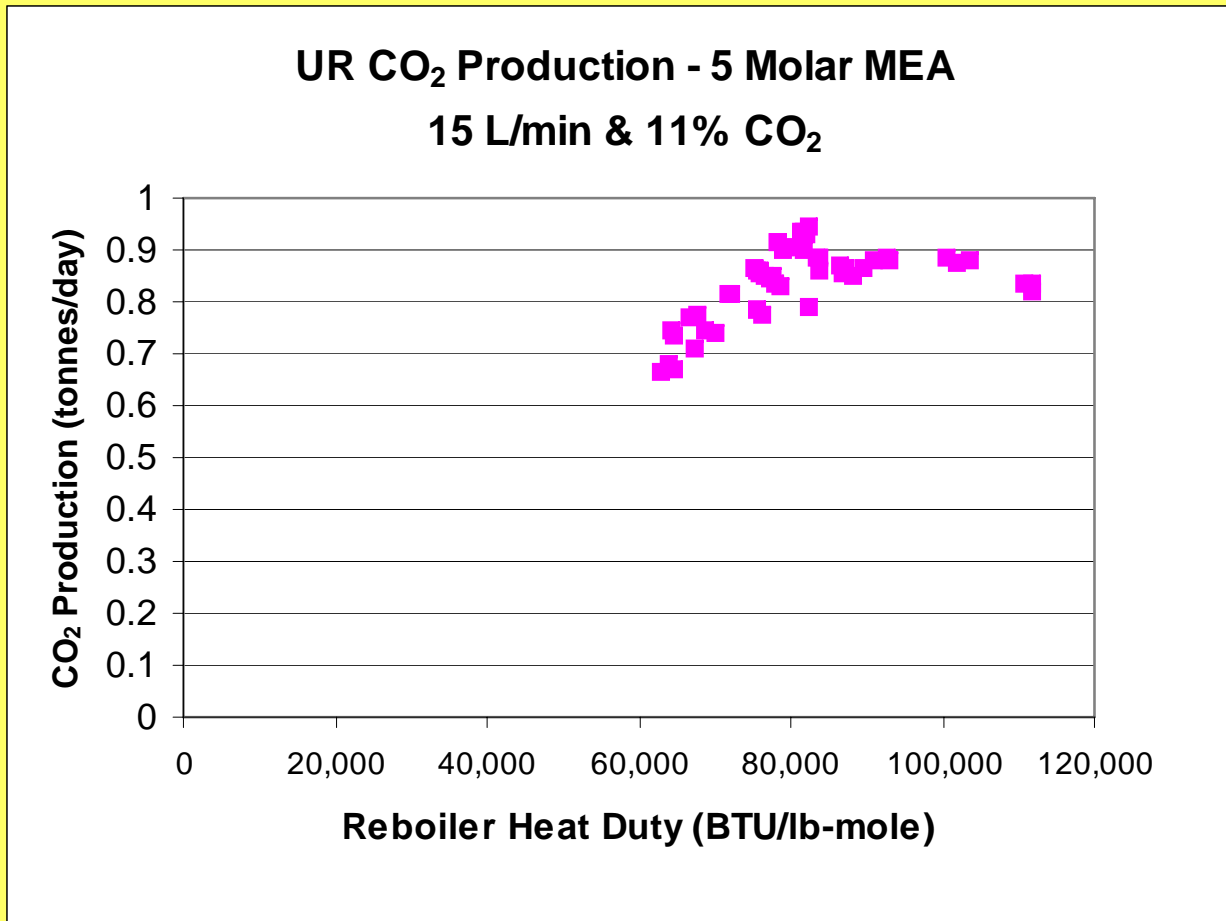
Some selected results from  
ITC Phase I



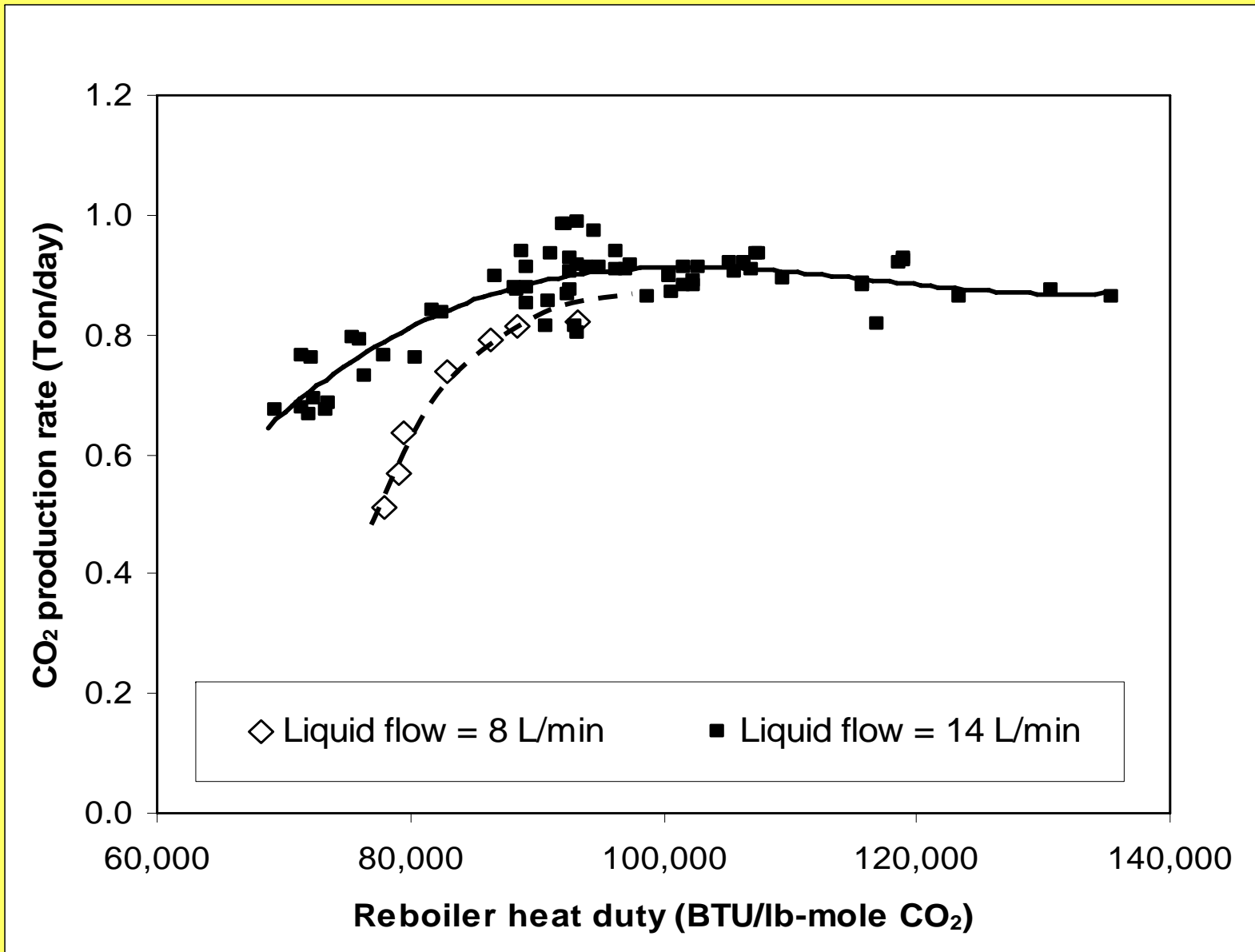
# Solvents and Technologies

- *Fluor Solvent Technology*
  - *(standard and current technology – 5M MEA with additives)*
- *Extra high concentrations*
  - *(7 to 9 M)*
- *Formulated solvents (MEA/MDEA mixtures)*

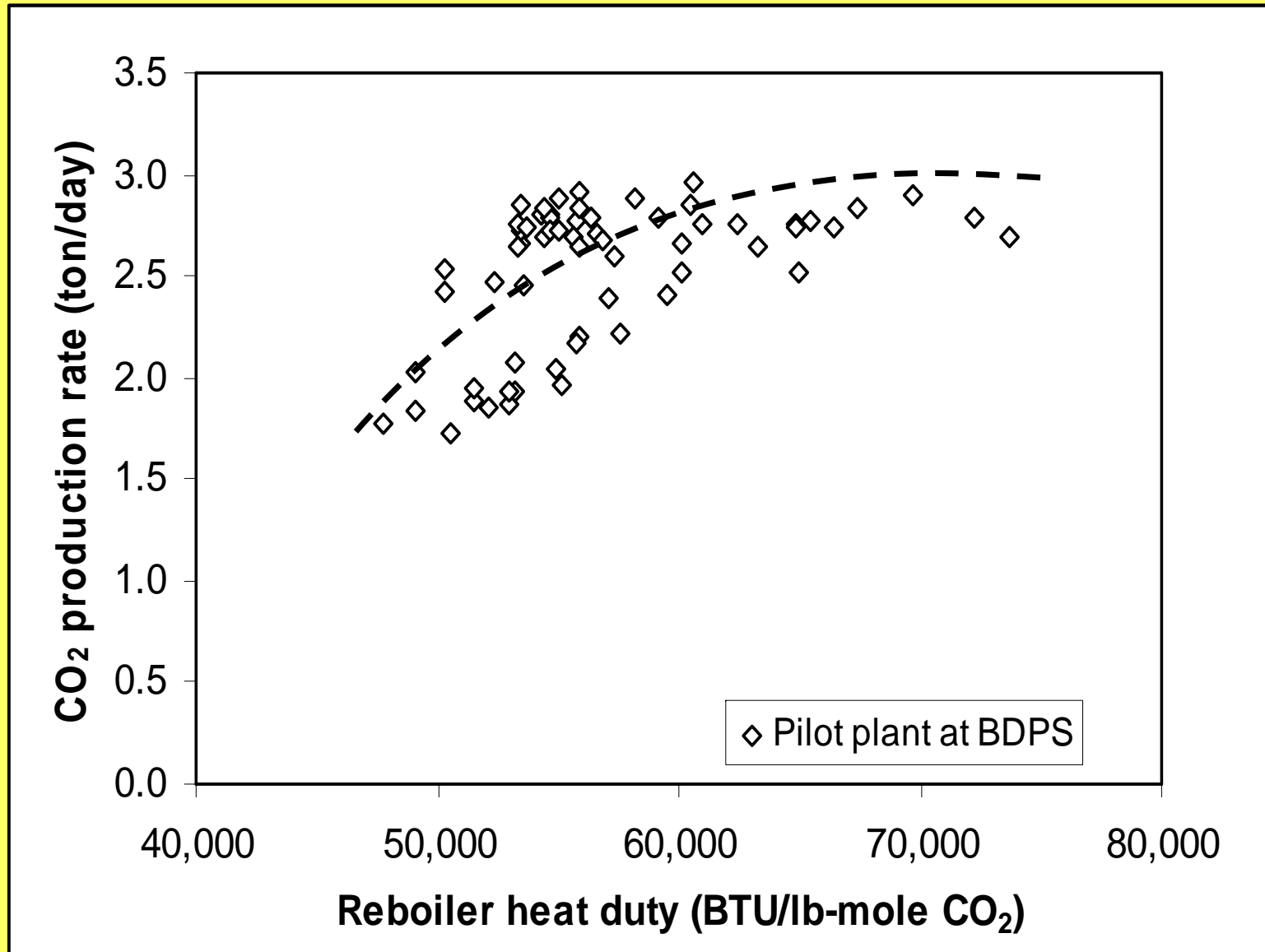
# UR CO<sub>2</sub> Production: Effect of Increasing Reboiler Heat Duty



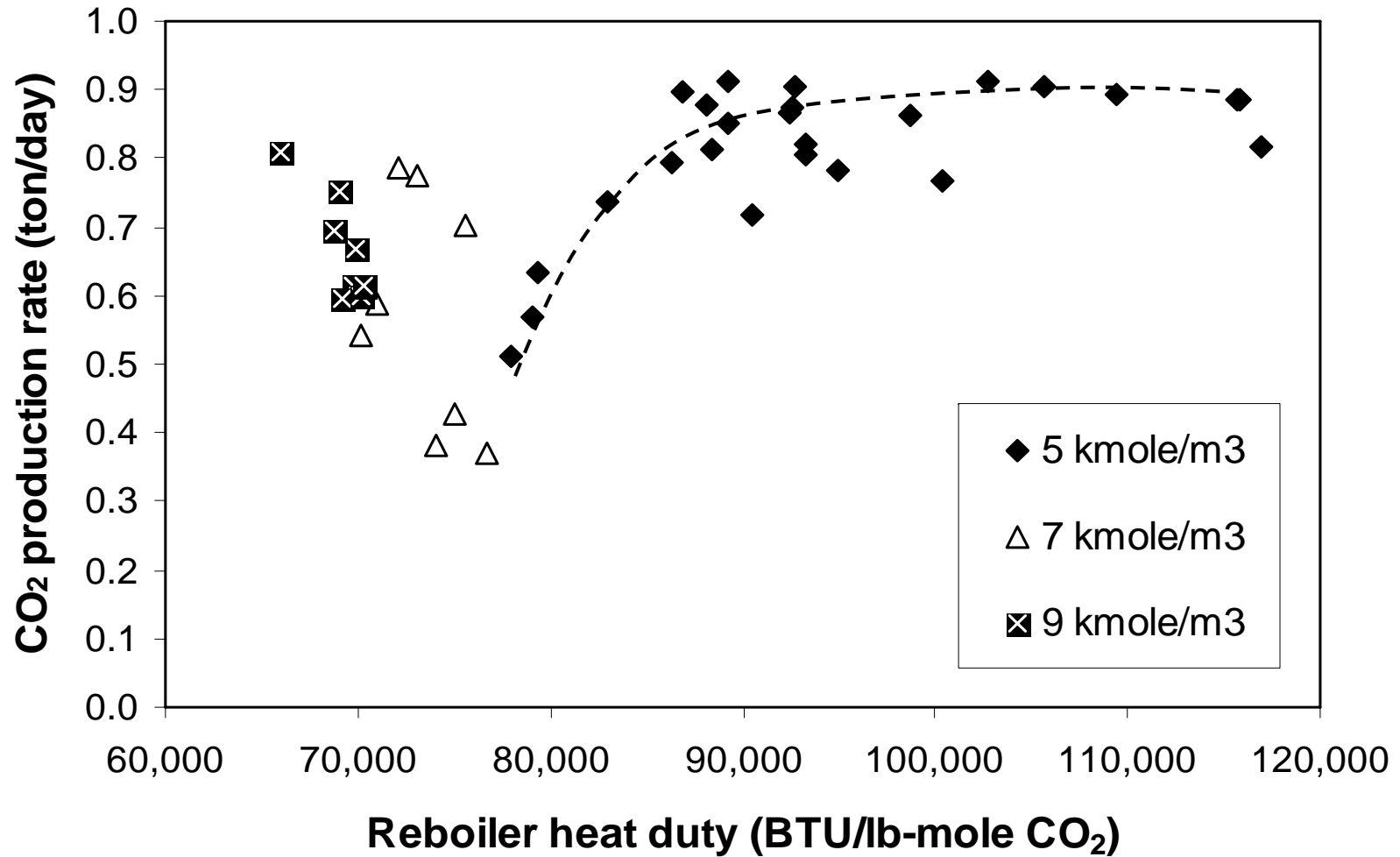
## UR Pilot Plant (5 kmol/m<sup>3</sup> MEA)



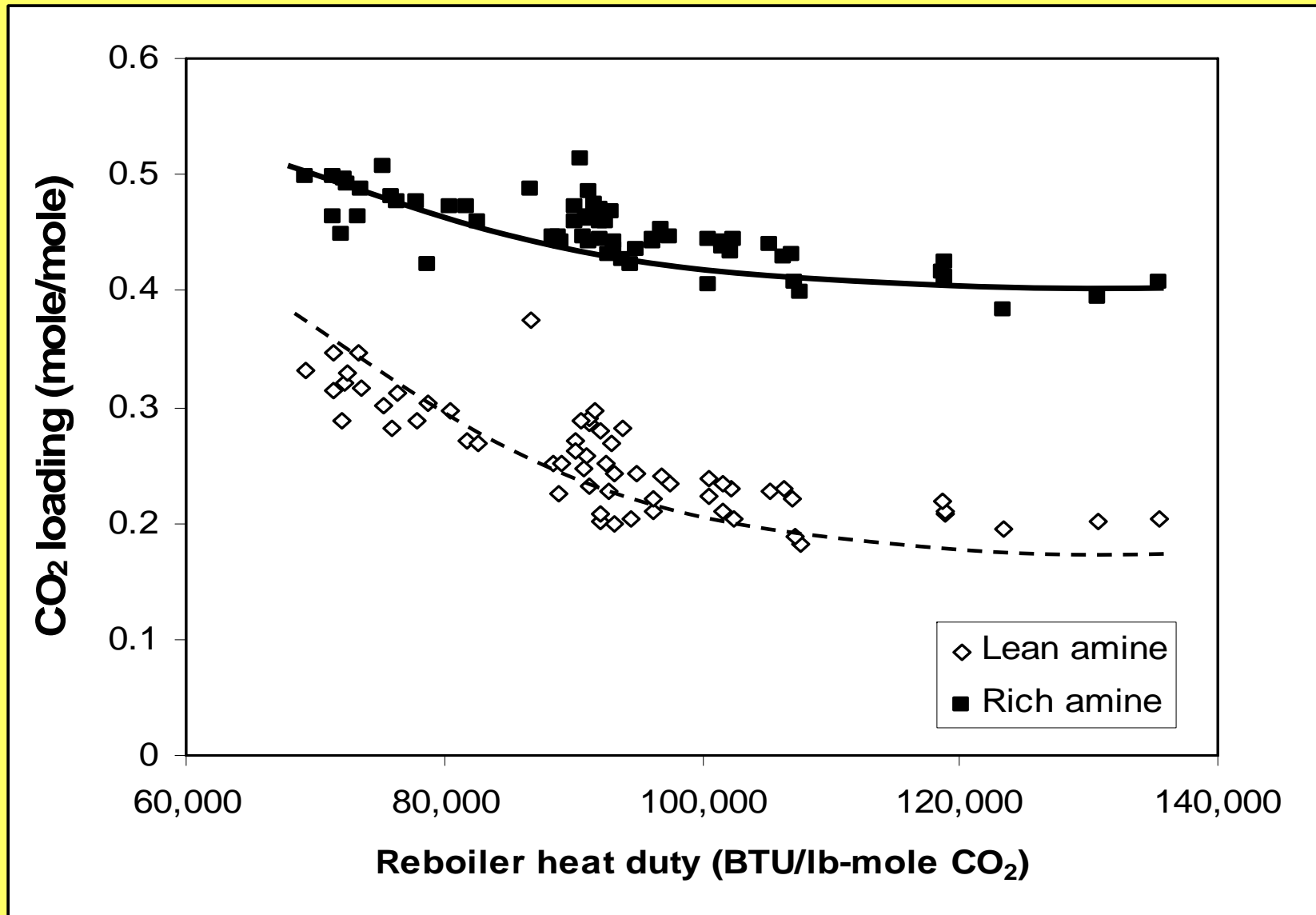
## BDPS Pilot Plant (5 kmol/m<sup>3</sup> MEA)



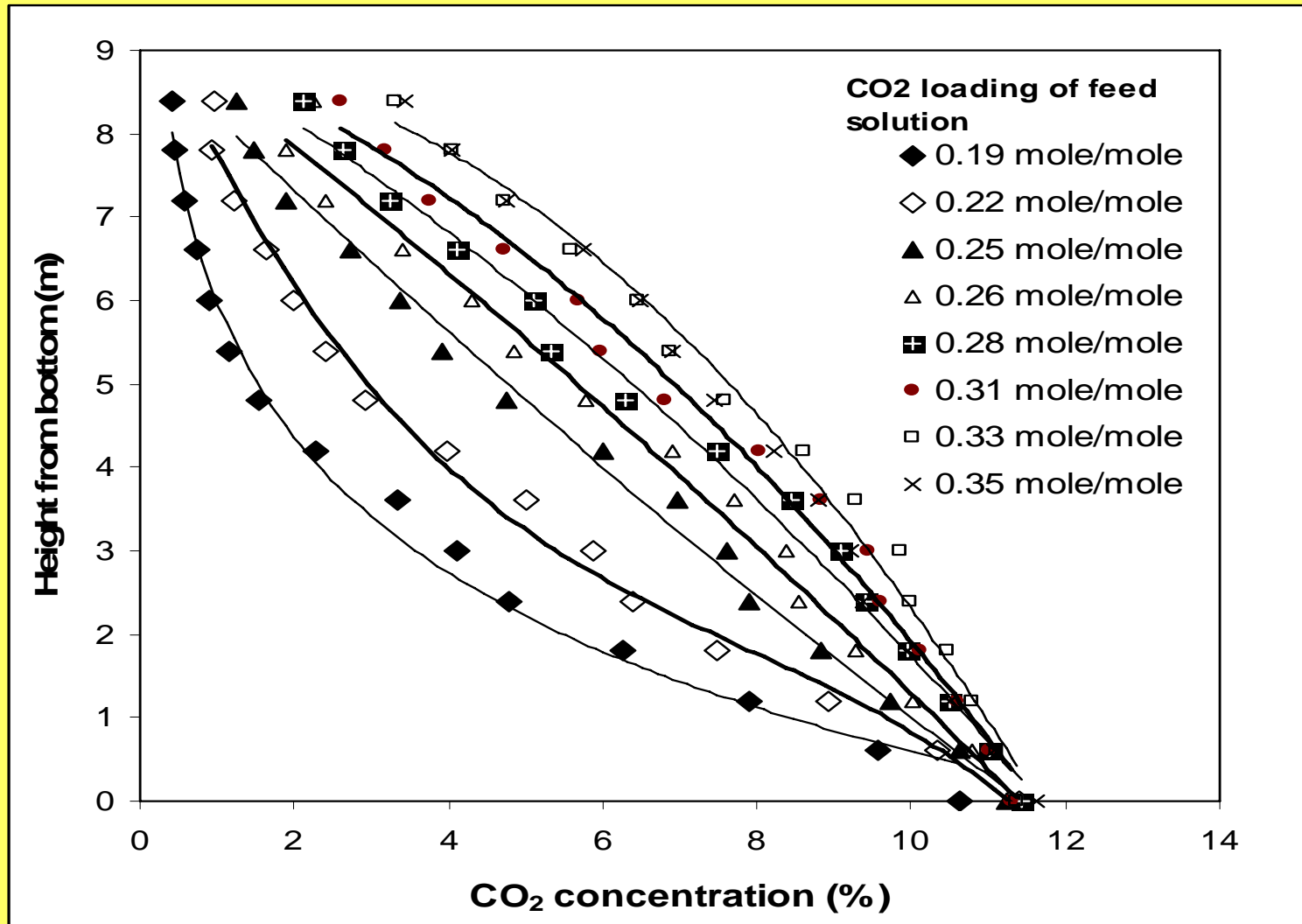
## Effect of Solvent Concentration



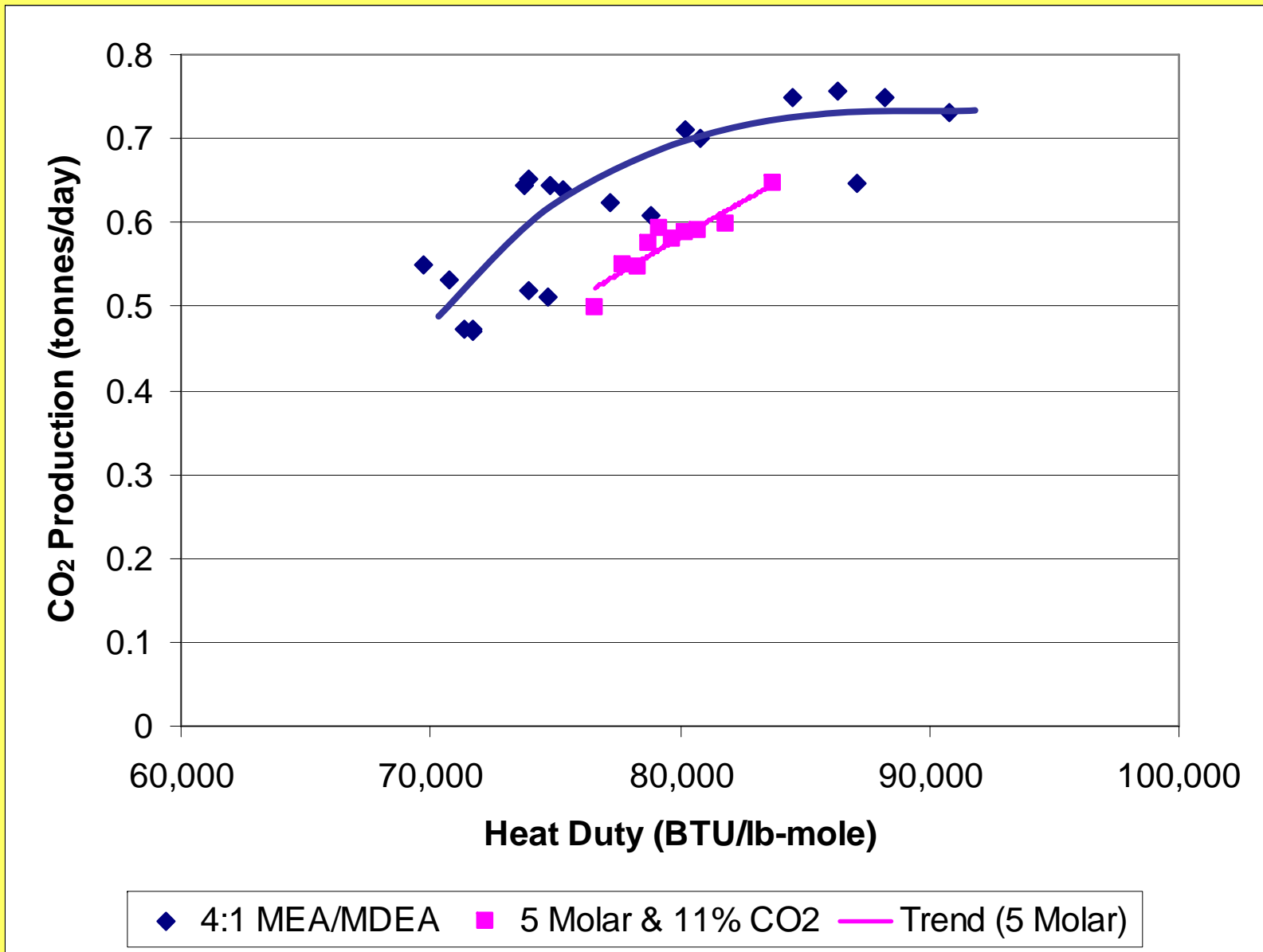
# Effect of CO<sub>2</sub> Loading in Reactive Solutions



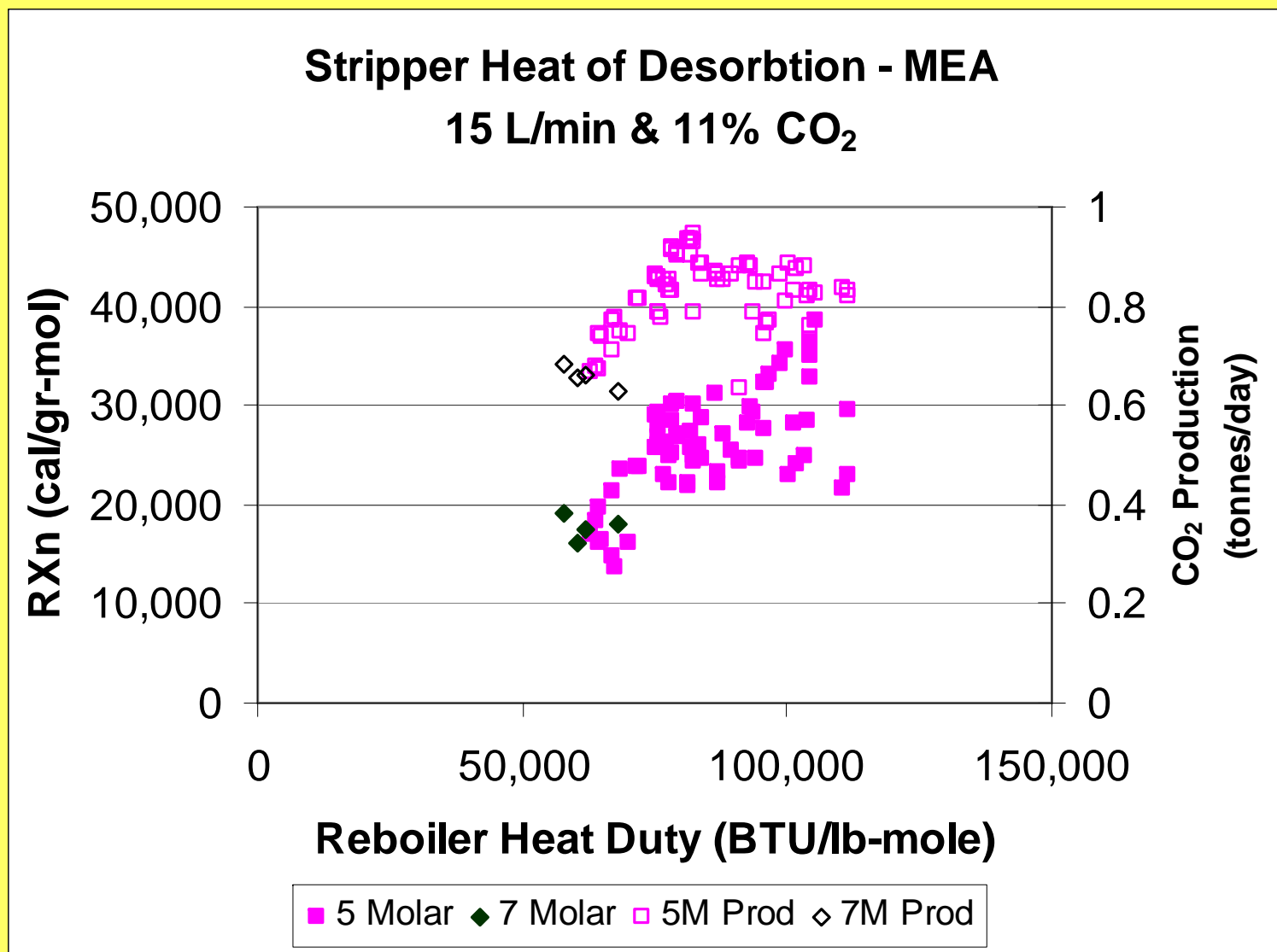
# CO<sub>2</sub> Concentration Profiles (UR Pilot Plant Studies)



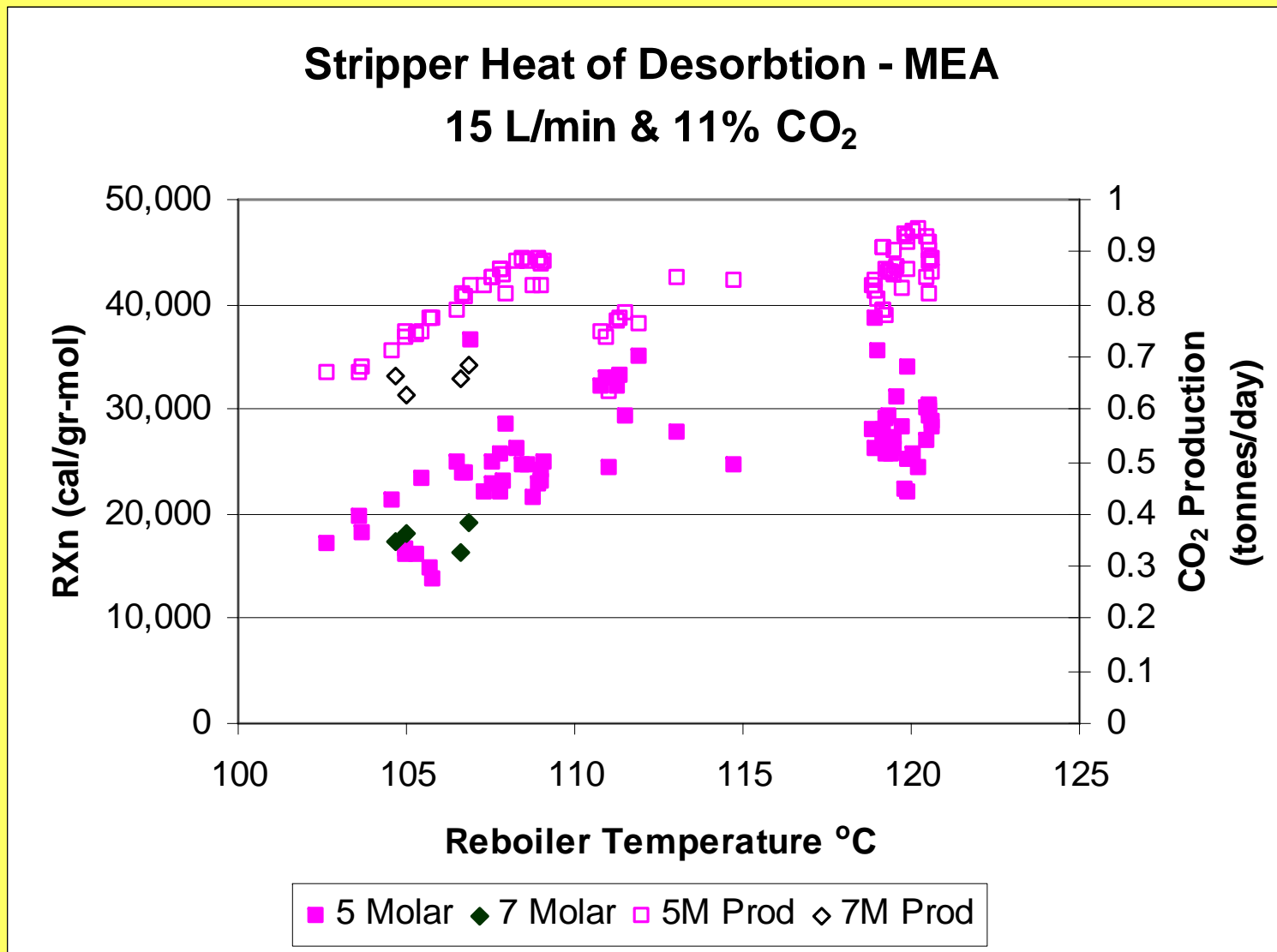
# CO<sub>2</sub> Production using 4:1 MEA/MDEA Mixed Solvents



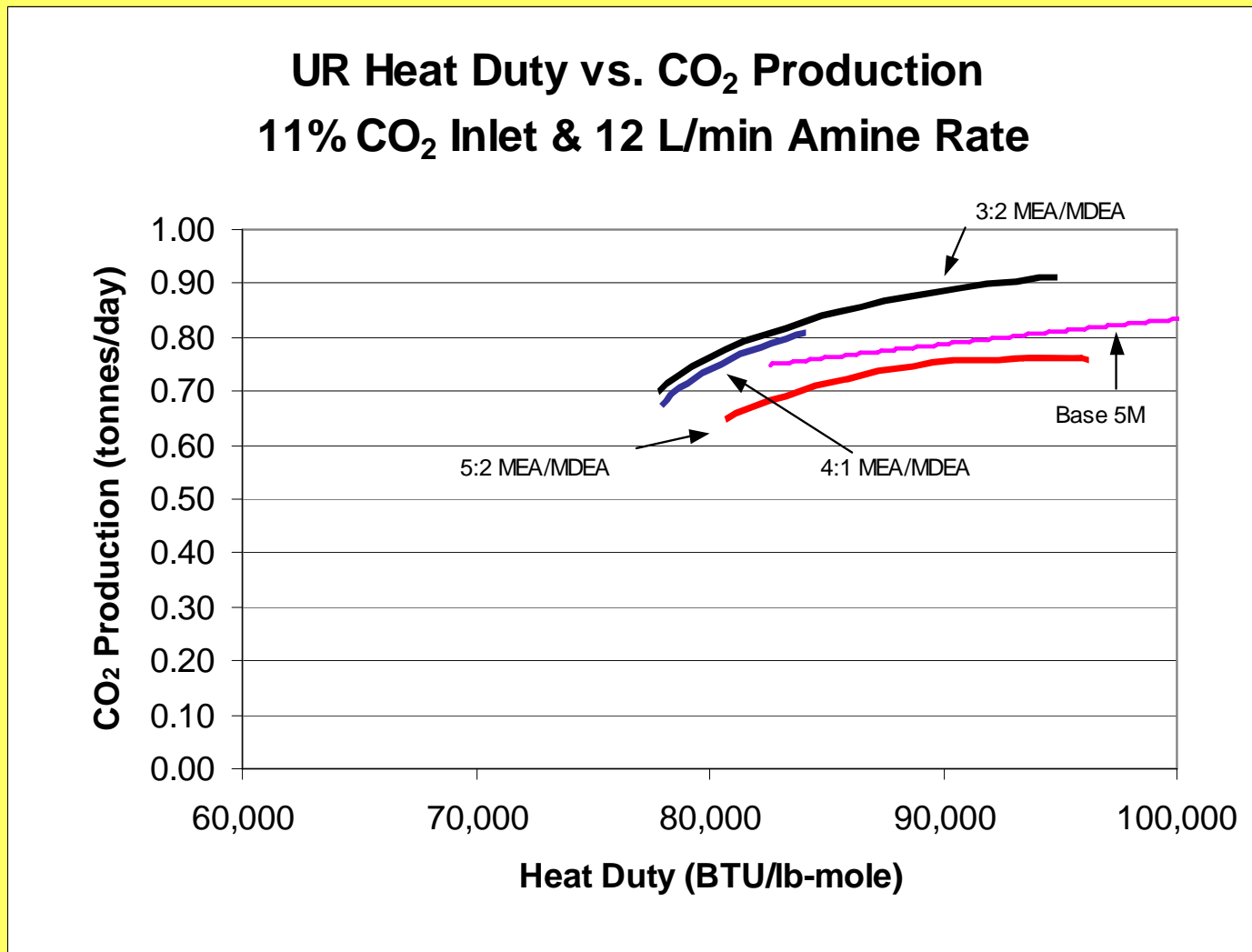
## Comparison of Stripper Heat of De-sorption and Production over Heat Duty Range



# Effect of Stripper Heat of Desorption and Production over Reboiler Temperature Range

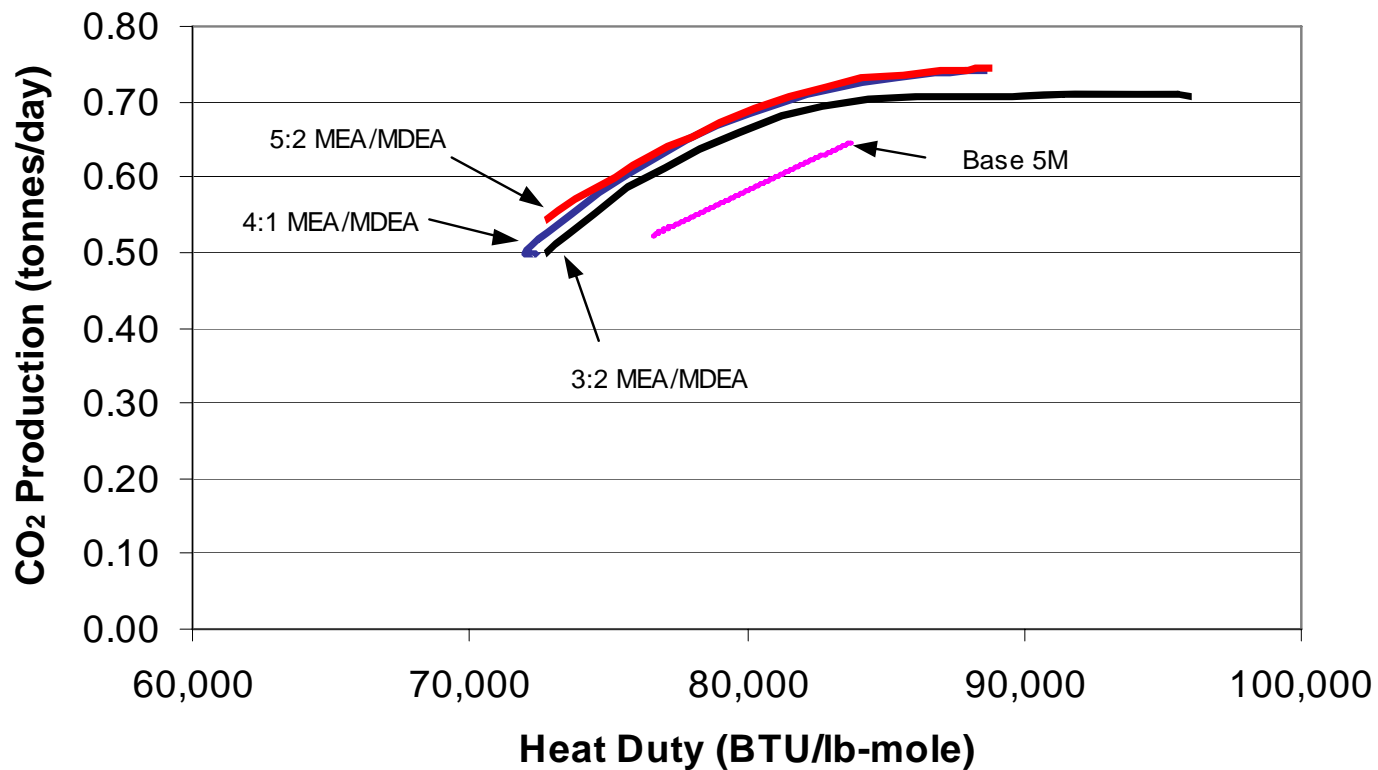


# UR CO<sub>2</sub> Production with MEA/MDEA vs. Reboiler Heat Duty

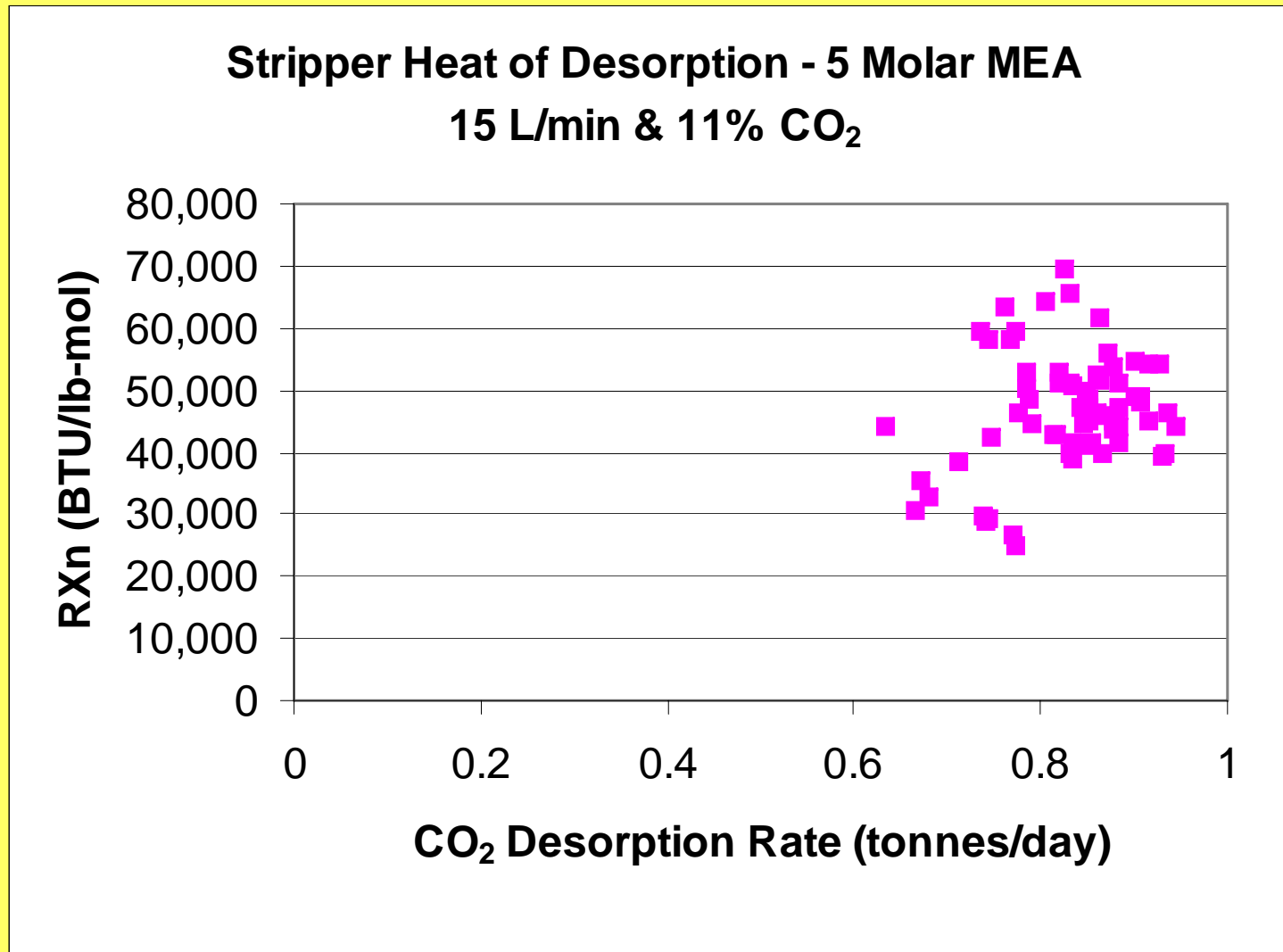


# UR Mixed MEA-MDEA Solvents: CO<sub>2</sub> Production as a Function of MEA/MDEA ratio

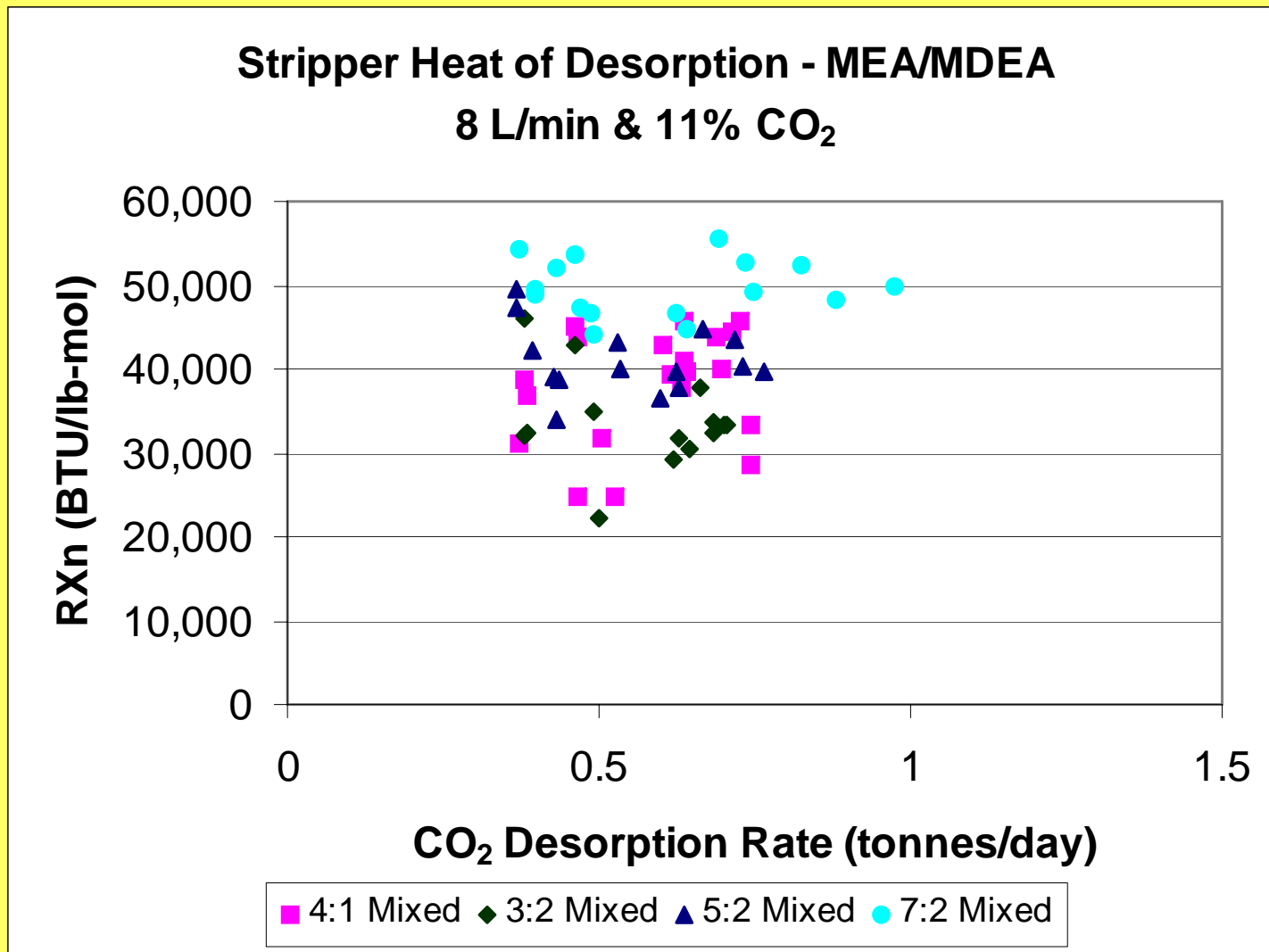
**UR Heat Duty vs. CO<sub>2</sub> Production  
11% CO<sub>2</sub> Inlet & 8 L/min Amine Rate**



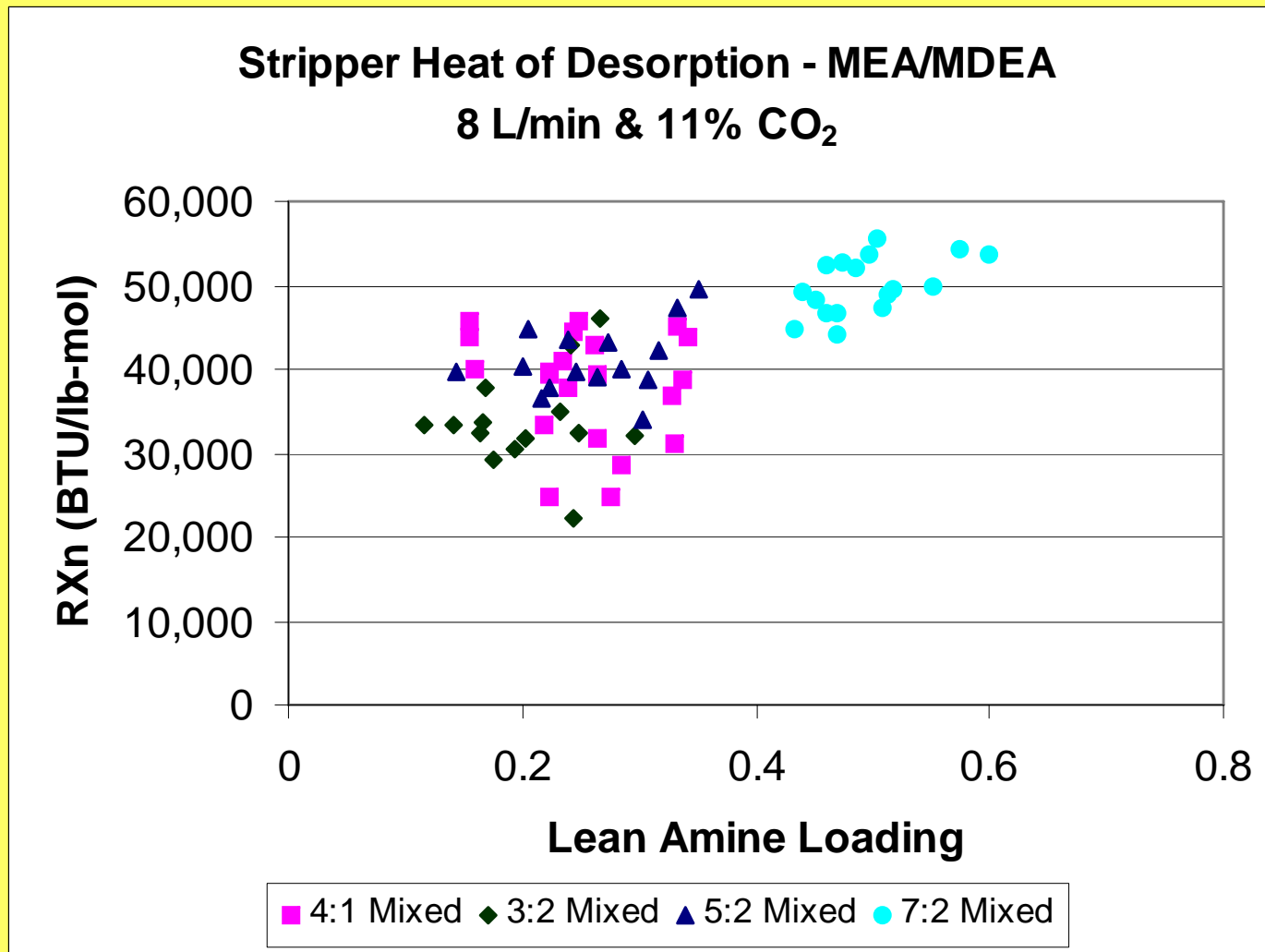
# UR Stripper Heat of Desorption vs. Production Rate



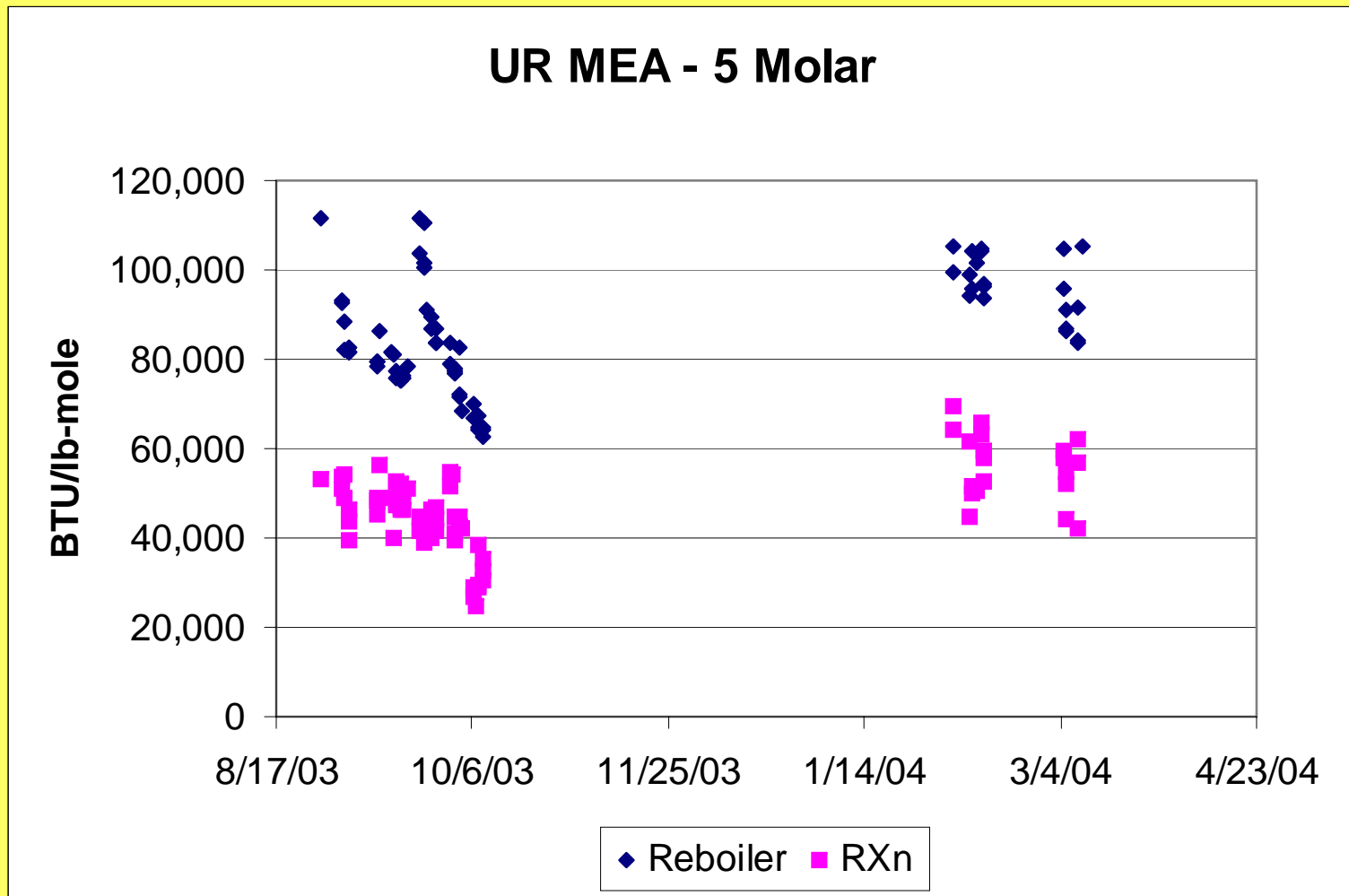
# UR Stripper Heat of Desorption vs. Production Rate



# UR Stripper Heat of Desorption vs. Lean Loading



# Reboiler vs. Stripper Desorption Energy Comparison



ITC Phase II :  
Work Plans (2005 – 2009)



# Task 1



- Significantly reduce the base and optimized cost of using “Designer Solvents” for CO<sub>2</sub> capture processes:
  - *Extra high concentration solvents with additives*
  - *Formulated mixed solvents*
  - *Designer solvents (e.g. PSR, etc.)*
  - *Novel Solvents developed by the University of Regina*



## Task 2

- Optimize process conditions/procedures through:
  - *modifications made to the operating conditions of the conventional MEA process*
  - *modifications made to the process configuration such as split flow and steam injection*



## Task 3

- System analysis and integration of promising technologies, process configurations, and operating procedures
  - *Examine improved technologies such as designer solvents, split-flow configuration, steam injection, and heat recovery to determine integration feasibility and practicality prior to pilot plant testing*

# Task 4



- Investigate opportunities to integrate solvent based CO<sub>2</sub> capture systems into existing and new Power Generation stations by:
  - *simulating a new power plant with the improved CO<sub>2</sub> capture process*
  - *identifying power plant waste heat sources suitable for use in CO<sub>2</sub> capture plant*

# Task 5 & 6

- Complete unit cost analysis for amine unit as well as integrated power plant / capture unit
- Continued evaluation of operational issues such as corrosion, solvent degradation, and process control strategies.



# Task 7 & 8

- Develop training package of the effective operation of a CO<sub>2</sub> capture module for pulverized coal power plants
- Investigate CO<sub>2</sub> product delivery and transport systems for optimization opportunities



# Long term directions

- Process technologies
  - Column packings
  - Process integration issues
  - Process configuration issues
- Solvents technologies
  - Current solvents (FID, etc.)
  - Generic mixed solvents
  - New class of solvents
- Integrated Modeling and Simulation
  - Integrated modeling for power and CO<sub>2</sub> productions
  - Comprehensive cost studies



# *New class of solvent technologies*

- *Formulated solvents (3 or more components, etc.)*
- *Sterically hindered amines*
- *Poly-structure amines*
- *New molecular design solvents*
- *Etc.*



# *Fundamental Research at ITC*



[www.uregina.ca](http://www.uregina.ca)



[www.co2-research.ca](http://www.co2-research.ca)

## *Research Program*

- High Performance Structured Packings
- New Formulated Gas Treating Solvents
- Rate Enhancement Mechanisms & Reaction Kinetics of Mixed Amines
- Solvent Stability (Degradation) Studies
- Corrosion Control
- Co-generation Applications
- Process Integration



# *Fundamental Research*



- ❖ *Solvent formulation*
- ❖ *Solvent reaction & kinetics*
- ❖ *Thermodynamics*
- ❖ *Column hydrodynamics*
- ❖ *Solvent stability*
- ❖ *Mass transfer with chemical reactions*
- ❖ *Corrosion control and prevention*
- ❖ *Co-generation Applications*
- ❖ *Process Integration*
- ❖ *Intelligent monitoring, planning and control systems*

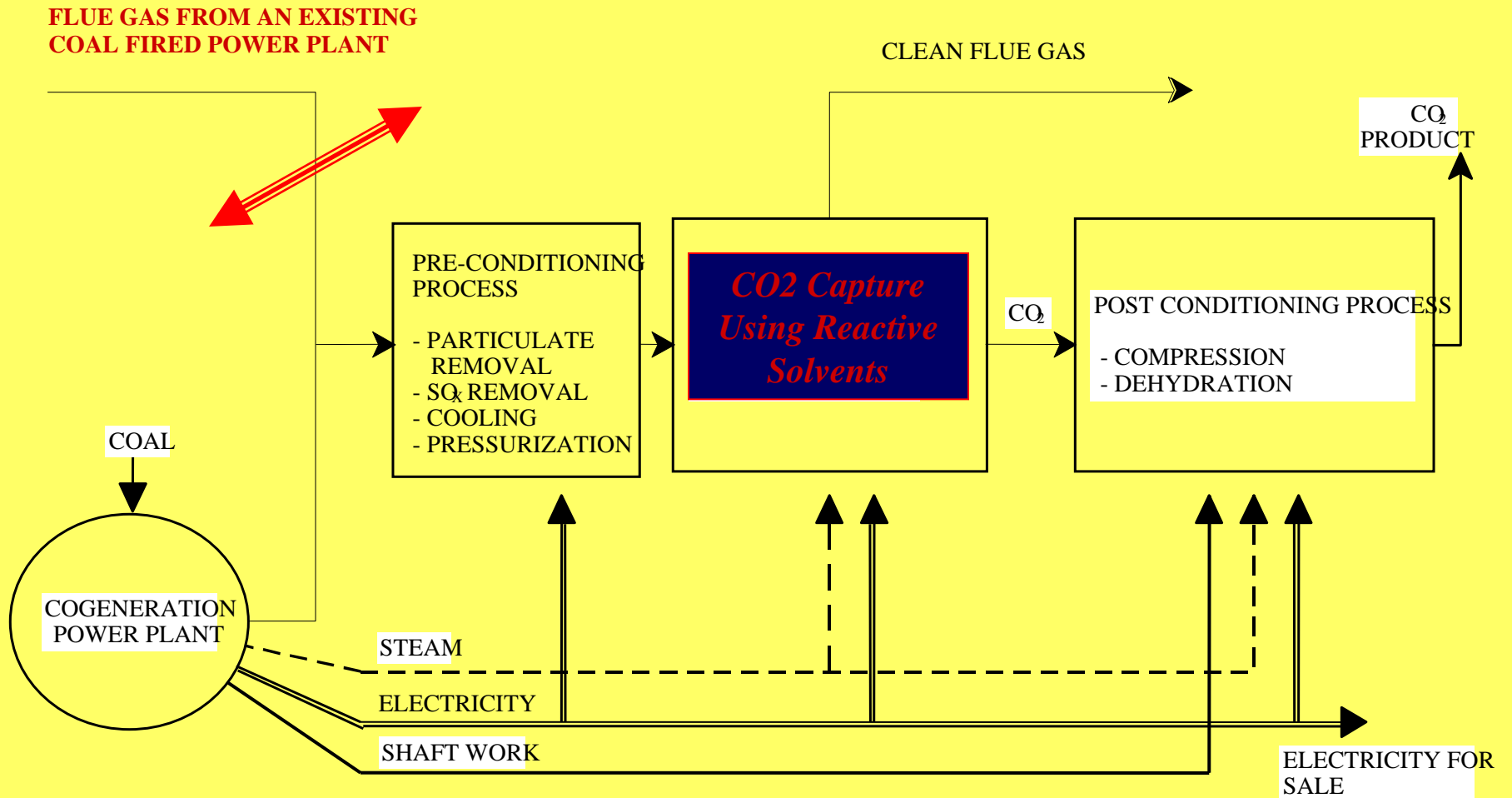
# Why use reactive solvents for CO<sub>2</sub> capture?

- Theoretical issue
  - Mass transfer of CO<sub>2</sub> in liquid is 10 to 100 times faster
- Proven technology
  - Use in gas processing
- Available today !
- Cost ~ \$25 to \$50 per ton of CO<sub>2</sub> (*depending on situation and location*)
  - CO<sub>2</sub> for EOR ~ \$20 to \$100 per ton of CO<sub>2</sub>
  - CO<sub>2</sub> trading ~ \$15 to \$35 per ton of CO<sub>2</sub>

# CO2 Life-cycle Analysis: “Green oil” from CO2 for EOR application

	CO2 Emission: Life-cycle analysis
<i>Primary oil production (reference case)</i>	<i>1.0</i>
<i>Secondary oil productions and Oil from Tar Sand Projects</i>	<i>1.25 to 1.5</i>
<i>“Green” Oil from CO2 – EOR applications</i>	<i>0.5 to 0.75 (50% to 100% less CO2)</i>

# Flexibility of Post-combustion Capture



*Thank You !*



[www.uregina.ca](http://www.uregina.ca)



[www.co2-research.ca](http://www.co2-research.ca)